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# Preparation and Catalytic Activity of Thermosensitive Ga<sub>2</sub>O<sub>3</sub> Nanorods

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**Supporting Information** 

ABSTRACT: Gallium oxide ( $\beta$ -Ga<sub>2</sub>O<sub>3</sub>) nanorods were prepared by ultrasonic irradiation of molten gallium in warm water to form  $\alpha$ -GaO(OH). This precursor was then subjected to calcination in air at 600 °C for 3 h to form  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>, as confirmed by Xray diffraction (XRD). Field emission scanning electron microscopy (FE-SEM)/high-resolution transmission electron microscopy (HRTEM) micrographs revealed the formation of well-organized nanotubes/nanorods with homogeneous size distribution. The average length of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods was affected by the temperature of the water during sonication, decreasing from 480 to 72 nm with an increase in the temperature from 25 to 50 °C. A sharp decline in the particle size was also observed when the temperature was above 35 °C. The catalytic activity of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods was examined, as a model, during the dehydration reaction of xylose to furfural. Furfural is a versatile biomass-derived platform compound used for the synthesis of several strategic chemicals. This nanoscale catalyst has a large surface area, which enhances its catalytic activity and enables it to completely convert xylose to furfural at 150 °C within 12 h without any trace of byproducts, as confirmed by highperformance liquid chromatography (HPLC), <sup>13</sup>C nuclear magnetic resonance (NMR), and <sup>1</sup>H NMR. The XRD pattern of the used  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods was identical to that of pristine Ga<sub>2</sub>O<sub>3</sub>, indicating the possible reusability of this catalyst.  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> was reused for more reduction cycles, with similar results to the freshly prepared  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>. HPLC analysis demonstrated that the selectivity of furfural is up to 94% compared to the 30% obtained with GaO(OH) as a catalyst.

# 1. INTRODUCTION

Nanoscale metals and nanosized metal oxides (MOs) exhibit unique physicochemical properties, functionality, and biocompatibility for a plethora of applications, including photonics, sensors, and catalysis.<sup>1–3</sup> Of particular interest is gallium oxide (Ga<sub>2</sub>O<sub>3</sub>), a chemically and thermally stable semiconductor with a wide bandgap of 4.9 eV. Its photocatalytic activity has been examined for water splitting, CO<sub>2</sub> photoreduction, and wastewater treatment.<sup>4</sup> Other applications include gas sensing,<sup>5,6</sup> photocatalysis,<sup>7</sup> optoelectric devices,<sup>4</sup> and polarized Xray absorption imaging.<sup>8</sup> Ga<sub>2</sub>O<sub>3</sub> also acts as an insulating barrier for spin-dependent tunneling junctions.<sup>9</sup> Its precursor GaO-(OH) is also an effective photocatalyst, similar to the popular and effective TiO<sub>2</sub>. The hydrothermal reaction of gallium with water at various temperatures has been reported for the synthesis of  $\alpha$ -GaOOH in the presence of oxalic acid.<sup>10</sup>

The dehydration reaction of GaO(OH) into Ga<sub>2</sub>O<sub>3</sub> occurs at elevated temperatures<sup>4,11,12</sup> via various synthetic routes: ball milling,<sup>13</sup> microwave treatment,<sup>14</sup> and the sonochemical reaction<sup>15</sup> of gallium.<sup>3,6–8</sup> Ga<sub>2</sub>O<sub>3</sub> has several morphologies, depending upon the preparation procedure. For instance, the laser ablation method provides GaO(OH) of spindle-like and nanofiber form, which produces Ga<sub>2</sub>O<sub>3</sub> nanorods upon dehydration.<sup>11</sup> A combined procedure of laser ablation followed

by reflux in the presence of cetyltrimethylammonium bromide or polyvinylpyrrolidone produces a mixture of GaO(OH) and  $Ga_2O_3$  nanowires.<sup>16</sup>

In the design of surface-exposed polymer–MO core–shell species, the core–shell must be easily accessed by the surrounding medium, a prerequisite for catalysis and sensing applications.<sup>17–20</sup> Stimuli- and thermoresponsive gallium-based oxides have been used as anchors for metal nanoparticles (NPs).<sup>18</sup> However, aggregation often compromises the performance of MO NPs. Therefore, the development of a convenient way to control the density of MO NPs with high precision is of uttermost importance.

The current research focuses on two main strategies: (a) the use of a heterogeneous as well as a selective acid catalyst and (b) the improvement of the process of furfural production from xylose. Solid catalysts are most often used because they show potential for advancement beyond current state-of-the-art methods. Moreover, they can be easily separated via simple filtration. The catalysts must display surface acidity, product selectivity through textural property adjustment, and enhanced

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# Table 1. Summary of the Literature Reports on the Production of Furfural from Xylose Using Various Catalysts

type of catalyst/ method for furfural production	solvent/catalyst	reaction conditions (time/temperature)	furfural yield (%)	reference
homogeneous/ microwave	HCl + NaCl/FeCl <sub>3</sub> in water	15 min, 200 °C	90	26
homogeneous/ hydrothermal	$\rm H_2SO_{4*}~NaCl/FeCl_3$ in water/toluene atmospheric pressure (boiling)	5 h, 170–185 °C	83	29
homogeneous/ hydrothermal	biphasic organic/SO <sub>3</sub> H <sup>-</sup> acid ionic liquid	1 h, 100 °C	85	30
homogeneous/ hydrothermal	$\rm EMIM/H_2SO_4$ [1-ethyl-3-methylimidazolium hydrogen sulfate ([EMIM][HSO_4])] in water/toluene	6 h, 180 °C	84	27
hetrogeneous/ hydrothermal	water/toluene; H-faujasite Si/Al = 15	6 h, 170 °C	90-95	31
hetrogeneous/ hydrothermal	mixed solvents (water/dimethyl sulfoxide/tetrahydrofuran); $\beta$ zeolite	6 h, 200 °C	42	32
hetrogeneous/ hydrothermal	water, dimethyl sulfoxide (DMSO), and a mixture of water and toluene (water/ toluene); H-zeolites	4 h, 140 °C	25	33
hetrogeneous/ hydrothermal	water/toluene; layered zeolite Nu-6(1)	4 h, 170 °C	47	34
hetrogeneous/ hydrothermal	water/toluene; Zr–W–Al mesoporous nanoparticles	2 h, 170 $^\circ \mathrm{C}$	50	35
hetrogeneous/ microwave	water; ZrO <sub>2</sub> -TiO <sub>2</sub>	5 min, 300 °C	10	36
hetrogeneous/ microwave	water/toluene; TiO <sub>2</sub> –graphene oxide	10 min, 170 $^\circ \mathrm{C}$	68	37
hetrogeneous/ hydrothermal	water; $\beta$ -Ga <sub>2</sub> O <sub>3</sub>	12 h, 170 °C	94 selectivity (66 wt %)	current study

hydrothermal stability.<sup>21</sup> The most studied solid acids are zeolites,<sup>22</sup> which are highly crystalline microporous inorganic aluminosilicates, containing channels with well-defined pores of 0.5-1.3 nm, in which the catalytic groups are located.<sup>23,24</sup> Zeolites based on aluminosilicate are strong acidic catalysts and show excellent thermal and chemical stability.<sup>23,24</sup> Branca et al. reported the acidic pyrolysis of corncobs for furfural production at 800 K in a packed-bed reactor using several catalysts, such as H<sub>2</sub>SO<sub>4</sub>, H<sub>3</sub>PO<sub>4</sub>, H<sub>3</sub>BO<sub>3</sub>, (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, ZnCl<sub>2</sub>, NiCl<sub>2</sub>, MgCl<sub>2</sub>, and  $Fe_2(SO_4)_3$ . The maximum yield of furfural production was 10%.<sup>25</sup> Marcotullio et al. studied the conversion of D-xylose to furfural in a solution of 50 mM HCl and NaCl at 200 °C, with 90% yield. They mentioned that the Cl<sup>-</sup> ions promote the formation of 1,2-enediol from the acyclic form of xylose.<sup>26</sup> Lima et al. found that the combination of 1-ethyl-3-methylimidazolium hydrogen sulfate ionic liquids and H<sub>2</sub>SO<sub>4</sub> provides the highest furfural yield of 85% from xylose at 180 °C.<sup>27</sup> However, the drawback of these methods is their inability to recycle the catalyst.<sup>26,27</sup> Recently, Mandalika et al. reported a reactive distillation batch process to produce furfural in excess of 85% of the theoretical yield based on pentose.<sup>28</sup> Ga<sub>2</sub>O<sub>3</sub> was not used in any of the previous reports as a catalyst for the conversion of xylose to furfural. However, some other catalysts were used for this reaction, as listed in Table 1.

The catalysts in Table 1 are representative examples from literature reports. It is worth noting that most of the published work on the conversion of xylose to furfural is based on the use of ionic liquids, zeolite-based materials, and MOs.

Furfural is a versatile biomass-derived platform compound for the synthesis of several strategic chemicals, which are currently derived from petroleum.<sup>38–41</sup> Xylose, obtained from the hydrolysis of hemicellulose, is an abundant and underutilized substrate. The conversion of pentose sugars to value-added products is still a key pending issue in biorefinery. In the current work, we describe a facile and efficient sonochemical pathway for the preparation of  $Ga_2O_3$  nanorods from molten Ga metal. The combined sonication and calcination techniques shorten the duration of the catalyst preparation (6 h) compared to conventional wet impregnation techniques. The  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> catalyst exhibits good activity and selectivity for the conversion of xylose to furfural. This solid catalyst can be easily separated from the product and reused. A proposed mechanism for the conversion of xylose to furfural is given.

#### 2. EXPERIMENTAL SECTION

**2.1. Chemicals.** Metallic gallium (99.999%) was purchased from Aldrich and used as received, and xylose and furfural were obtained from Sigma-Aldrich, Israel. Doubly distilled water (DDW) obtained from a TREION purification system was used in this work.

2.2. Experimental Design and Methods. The detailed ultrasonic formation of Ga particles in aqueous media was reported elsewhere.  $^{15,42-44}$  In brief,  $Ga_2O_3$  was prepared by immersing a granule of Ga (ca. 1.0 g) in  $\sim$ 20 mL of DDW, which was heated to 60 C, forming a liquid gallium phase at the bottom of the test tube. The system was irradiated for 3 h with ultrasonic energy at 65% amplitude [ultrasonic transducer model VCX 750, Sonics & Materials, Newtown, CT, performed at 20 kHz and 230 V alternating current (AC)], giving a white-gray suspension, which turned into white flakes as the sonication proceeded. The resulting product was separated by centrifugation, dried in vacuum, and calcined at 600 °C under an ambient atmosphere in a muffle furnace. The conversion of xylose to furfural by Ga<sub>2</sub>O<sub>3</sub> was performed at 150 °C for 12 h with a catalyst/ xylose ratio of 1:1 (wt %). The reaction products were analyzed by <sup>1</sup>H and <sup>13</sup>C nuclear magnetic resonance (NMR) [300 MHz NMR (Bruker)] and a high-performance liquid chromatography (HPLC) chromatogram. The catalytic reactions were performed in water using a Teflon-lined stainless-steel autoclave [100 mL, stainless-steel autoclaves with a polytetrafluoroethylene (PTFE) hydrothermal synthesis reactor (MH-25) liner made in China] that contained a known amount of xylose (0.5-1 g) and  $Ga_2O_3$  (0.05-0.5 g) and 20 mL of distilled water. A hydrothermal treatment was carried out for 2-12 h in the temperature range of 120-150 °C. The experimental conditions (reaction duration and temperature and the xylose/catalyst ratio) were varied to find the best furfural yield. The time was measured starting from the point at which the temperature of the mixture reached the set value. At a certain point in time, the reaction



Figure 1. SEM micrograph of (a)  $\alpha$ -GaO(OH) and (b)  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>, (c) XRD of  $\alpha$ -GaO(OH), and (d) XRD of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>.

was quenched by cooling the autoclave in a water bath. Timedependent profiles were obtained by collecting the reaction results at different time points. The reaction mixture was centrifuged at 8000 rpm for 10 min at 15  $^{\circ}$ C, to separate the supernatant from the precipitate.

2.3. Analysis. Scanning electron microscopy (SEM) was performed using an Inspect FEI microscope. The samples were prepared by placing a small portion of the dried particles on a sample holder coated with carbon tape. For environmental scanning electron microscopy (ESEM) analysis, the sample surfaces were coated with a thin evaporated carbon layer for conductivity. Transmission electron microscopy (TEM) was performed using Tecnai G2, FEI, high contrast/cryo-TEM, (Hillsboro, OR), equipped with a bottom chargecoupled device (CCD) camera,  $1000 \times 1000$ . For TEM imaging, the particle-containing sample was dispersed in isopropanol and subjected to bath sonication. Three small droplets from the resulting suspension were then applied to a carbon-coated copper TEM grid and dried under vacuum in a covered Petri dish. Ultraviolet-visible (UV-vis) and diffusion reflectance spectra of materials were measured using a Cary 100 spectrophotometer (Varian), operated by Lab Sphere software. A Bruker D8 Advance and a Philips PW1050 X-ray diffractometer (Cu K $\alpha$  radiation, operating at 40 kV/30 mA with a 0.0019 step size and a 0.5 s step) were used for X-ray diffraction (XRD). HPLC analysis was carried out on a Merch-Hitachi LaChrom system L-7000 equipped with a L-7455 diode array detector and a Schambeck SFD R1 2000 refractive index detector, Bad Honnef, Germany, using a 300  $\times$  7.8 mm Rezex-ROA ion-exclusion chromatography column (Torrance, CA) equipped with a matching guard column.

#### 3. RESULTS AND DISCUSSION

**3.1.** Formation of GaO(OH) and Characterization of  $\alpha$ -GaO(OH) and  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>. The ultrasonic irradiation induced acoustic cavitation in water, causing the dispersion of molten gallium into micrometric spheres. Under irradiation, the gallium spheres turned into white crystallites of GaO(OH) via the reaction of the gallium particles with dissolved oxygen and OH<sup>•</sup> radicals that were formed by the partial decomposition of water.<sup>15</sup>

SEM images show that the  $\alpha$ -GaO(OH) crystallites are shaped as nanorods (Figure 1a), ca. 500–1000 nm long and ca. 50-100 nm wide. Their composition and crystallinity are confirmed by XRD analysis (Figure 1c). Sharp intense signals from the crystal planes, typical of orthorhombic GaO(OH), are observed (Figure 1c). The dominant peaks are reflections of the (110), (130), (111), and (240) planes at the  $2\theta$  angles of 21.5°,  $33.7^{\circ}$ ,  $37.2^{\circ}$ , and  $54.02^{\circ}$ , respectively. The crystallite sizes of GaOOH and Ga2O3 are calculated using Scheerer's equation and are found to be 17 and 18 nm, respectively. The density of the crystallites increases with the increase in sonication time (Figure S1 of the Supporting Information). Heating the  $\alpha$ -GaO(OH) crystallites to 600 °C does not induce changes in their shape (Figure 1b) but rather in their chemical composition. The XRD pattern matches crystalline  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> (Figure 1d) with its monoclinic phase [Joint Committee on Powder Diffraction Standards (JCPDS) 41-1103]. The crystal structures of  $\alpha$ -GaO(OH) and  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> were calculated on the basis of XRD analysis and are presented in Figure S2 of the Supporting Information [orthorhombic phase for GaO(OH)



Figure 2. TEM images of (a)  $\alpha$ -GaO(OH) (inset: SAED), (b)  $\alpha$ -GaO(OH) (inset: magnified image of a single particle), and (c)  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> (inset: SAED) and (d) HRTEM images of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> (inset: well-resolved lattice fringes).

and monoclinic phase for  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>]. TEM and high-resolution transmission electron microscopy (HRTEM) images of  $\alpha$ -GaO(OH) crystallites (after sonication of the molten Ga) are shown in panels a and b of Figure 2. The inset in Figure 2a shows the selected area electron diffraction (SAED) pattern of  $\alpha$ -GaO(OH) with an orthorhombic crystal structure. Detailed analysis of the crystal structure was reported elsewhere.<sup>15</sup> A TEM image of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> crystallites is shown in Figure 2c, together with their SAED. The ring pattern reflects the polycrystalline nature of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> product. HRTEM images of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> particles are shown in Figure 2d. The observed *d*-spacing value for  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> is 0.36 nm, which fits well with the spacing of the monoclinic phase of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> plane. The elemental composition of the calcined product was also examined by energy-dispersive spectroscopy (EDS) (Figure \$3 of the Supporting Information), and the presence of Ga and O without any impurities was confirmed (Figure S3 of the Supporting Information). Two elements observed on the spectrum, C and Cu, originated from the copper grid and the carbon tape, respectively.

Characteristic UV absorption bands were observed at 210 and 256 nm for  $\alpha$ -GaO(OH) and  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>, respectively (Figure S4a of the Supporting Information).  $\alpha$ -GaO(OH) displayed no obvious absorbance at wavelengths up to 210 nm, indicating high transparency under UV light. For further conformation, we have used diffused reflectance spectroscopy. Both of these techniques, namely, UV–vis and diffused reflectance spectroscopy, use UV–vis light excited valence electrons to empty orbitals. The difference in these techniques is that, in UV–vis spectroscopy, the relative change of transmittance of light is measured as it passes through a solution, whereas in diffuse reflectance, the relative change in the amount of light reflected off a surface is examined. Analogous to the UV–vis spectra, a typical reflectance band is observed at 211 nm in the case of  $\alpha$ -GaO(OH) and at 256 nm in the case of Ga<sub>2</sub>O<sub>3</sub>.

Furthermore, dynamic light scattering (DLS) and  $\zeta$  potential measurements were performed to probe the surface charge and particle size distribution of the  $\alpha$ -GaO(OH) and  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods. The  $\alpha$ -GaO(OH) nanorods exhibit a  $\zeta$  potential of -40.4 mV (Figure S5a of the Supporting Information) and a homogeneous size distribution. The hydrodynamic diameter of  $\alpha$ -GaO(OH) decreases from 460 to 110 nm with the increase in the temperature from 25 to 50 °C (panels a and b of Figure 3).

At 20 °C, the hydrodynamic diameter of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods was about 480 nm with a corresponding  $\zeta$  potential of -41.7 mV (Figure S5b of the Supporting Information), which is similar to the length of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods obtained in the corresponding TEM images (panels c and d of Figure 2). DLS measurements reveal a hydrodynamic diameter



Figure 3. DLS curve of  $\alpha$ -GaO(OH) at (a) 25 °C and (b) 50 °C, DLS plot of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> at (c) 25 °C and (d) 50 °C, (e) hydrodynamic size versus temperature, and (f) speculation of coagulation and decoagulation of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods.

of 480 nm for  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> at 25 °C and 72 nm at 50 °C (panels c and d of Figure 3). There is a sharp decline in the hydrodynamic size of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> at temperatures above 35 °C (Figure 3e). At 50 °C, the corresponding hydrodynamic diameter of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> nanorods is only 72 nm. The particles exhibit a homogeneous dispersion with a particle distribution index (PDI) of ~0.25. The stability and speculated structure is shown in Figure 3f.

3.2. Dehydration of Xylose to Furfural by  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>. Furfural was obtained from the dehydration of three water molecules dissociated from xylose by either liquid or solid acid catalysts.  $^{26,27}$  The use of  ${\rm Ga}_2{\rm O}_3$  as a catalyst helps to solve safety problems, such as the handling of strong acids, equipment corrosion, and waste treatment associated with strong acids. The reaction was carried out in an aqueous solution of xylose (0.17 M) at 150 °C for 12 h, and the formation of furfural was analyzed by <sup>13</sup>C NMR (Figure 4a). Thermosensitive Ga2O3 nanorods should have a small particle size and high surface area at this high temperature. As mentioned above, GaO(OH) can also catalyze this reaction. However, an appreciable amount of byproducts, including lactic acid, were detected when GaO(OH) was used as the catalyst. The reduced selectivity of GaO(OH) may be due to the basic sites (OH) present in this catalyst that promote the formation of lactic acid and other dehydration products. Nevertheless, furfural was formed with GaO(OH) as a result of the presence of the Ga<sup>3+</sup> Lewis acid. Furfural and other byproducts were further analyzed by <sup>1</sup>H NMR in corroboration with the <sup>13</sup>C NMR results (Figure S6 of the Supporting Information). Consequently, a series of experiments was conducted using Ga<sub>2</sub>O<sub>3</sub> to probe its loading effect. The amount of catalyst was varied between 0.5 and 0.1 g when dehydrating D-xylose (25 mg/mL) at 150 °C for 12 h. Both <sup>13</sup>C and <sup>1</sup>H NMR confirm



**Figure 4.** (a) <sup>13</sup>C NMR spectra of the product obtained from the hydrothermal reaction (12 h and 150 °C) with  $\alpha$ -GaO(OH) and with  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> and (b) HPLC evaluation of  $\alpha$ -GaO(OH) and  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> of the hydrolysate from p-xylose [conditions: 20 mL of neutral hydrolysate, 0.5 g of p-xylose, and 0.2 g of catalyst at 150 °C for 12 h; replicates of n = 3; error bars indicate standard deviation (SD)].





that the reaction was completed with a catalyst/xylose ratio of 1:1 and 0.4:1 (wt %) (Figure S7 of the Supporting Information). With further probing into the nature of the catalyst/xylose ratio (at lower ratios, 0.2:1 weight ratio), unreacted xylose was still detected after 12 h. Thus, 1:1 and 0.4:1 (wt %) ( $\beta$ -Ga<sub>2</sub>O<sub>3</sub>/xylose) ratios produce a high amount of furfural with higher selectivity than the 0.2:1 (wt %) ( $\beta$ -Ga<sub>2</sub>O<sub>3</sub>/xylose) ratio. As a result, the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>/xylose ratio of 0.4:1 (wt %) is chosen as the optimum, because this lower amount of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> enables high furfural production.

The quantification of the furfural product was performed using HPLC analysis. As shown in Figure 4b,  $Ga_2O_3$  is more active and selective for the dehydration of xylose to furfural than  $\alpha$ -GaO(OH). The superiority of  $Ga_2O_3$  is also reflected in the absence of any appreciable amount of byproducts, and the yield of furfural approaches 66 wt %. The selectivity toward the production of furfural reaches 94 and 30% for  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> and  $\alpha$ -GaO(OH) catalysts, respectively. The yield obtained using  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> is compared to that obtained using Nafion 117, which hydrates xylose in dimethyl sulfoxide at 150 °C with only 60% of the theoretical furfural yield.<sup>45</sup> Similarly, sulfonated graphene oxide (SGO) can be used for the dehydration of xylose to furfural in water with an average yield of 61%.<sup>46</sup> No reactive oxygen species (ROS) are expected to be involved in this reaction because  $Ga_2O_3$  does not produce ROS under room light.<sup>47</sup> Our previous study shows that blue light induces hydroxyl radical formation in  $Ga_2O_3$ , which is irrelevant to the current study.<sup>47</sup>

3.3. Postulated Dehydration Mechanism. Incomplete coordination of metal cations and oxide anions on the MO crystals facilitates the formation of acidic and basic sites on its surface. Thus, ionic MO surfaces are expected to contain coordinative unsaturated cations (Lewis acid sites) and basic sites. These Lewis acid sites that are exposed at the surface of the ionic oxides present a good opportunity for xylose (reducing sugar) to donate an electron to the metal cation to catalyze the reaction. Ga has an oxidation state of +3 in both  $Ga_2O_3$  and GaO(OH). We adopted a mechanism consistent with the previous findings<sup>48,49</sup> that Ga<sup>3+</sup> catalyzes the dehydration of xylose through a 1,2-hydride shift. Being a Lewis acid, Ga<sup>3+</sup> carries the reaction in the forward direction by converting emerging xylose into an oxocarbenium ion. At the final stage, the deprotonation of this species results in enol, and the subsequent loss of three water molecules produces furfural. The proposed reaction scheme is presented in Scheme 1.

The higher yield of furfural that was obtained with  $Ga_2O_3$  (66%), in comparison to GaO(OH) (22%), as illustrated in the HPLC results, can be explained by considering the role of the

Lewis acid sites in the catalysis.  $Ga_2O_3$  have two Ga atoms per molecule, whereas GaO(OH) has only one Ga atom per molecule. Because the catalytic activity is attributed to the  $Ga^{3+}$  ions, two Ga atoms provide a greater probability for D-xylose molecules to react on its surface and carry out the reaction in the forward direction than in the case of GaO(OH). Brunauer–Emmett–Teller (BET) also showed a higher surface area (17 m<sup>2</sup>/g) for Ga<sub>2</sub>O<sub>3</sub> than for GaO(OH) (10 m<sup>2</sup>/g). The increased surface area also promotes a strong interaction between xylose and Ga<sub>2</sub>O<sub>3</sub> compared to GaO(OH).

After the dehydration of xylose to furfural, used  $Ga_2O_3$  was separated from the reaction liquid and subjected to XRD analysis (Figure 5). The XRD pattern of used  $Ga_2O_3$  was



Figure 5. XRD pattern of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> catalyst before and after the reaction.

virtually identical to that of pristine  $Ga_2O_3$ . Moreover, SEM and TEM analyses were also carried out to probe the morphology of the used catalyst. No morphological changes were observed in the catalyst before and after the reaction (Figure S8 of the Supporting Information). Such a result provides a reason for the reuse of this solid catalyst and its application in a packed/fluidized-bed reactor for continuous processing and facilitated furfural recovery.

3.4. Reusability Study of the  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> Catalyst.  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> was reused to demonstrate the reusability of the catalyst for the production of furfural, and a similar result to that of freshly prepared  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> was obtained. The reusability of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> was tested for three reaction runs under optimal reaction conditions. To reduce the loss of catalyst material during separation and drying, the reaction product obtained in each case was separated from the catalyst by centrifugation. Fresh xylose and water were added to the residual solid that remained from the catalyst in the centrifugation tube. The contents were transferred to the hydrothermal reactor and subjected to 150 °C for 12 h. The effective reusability of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> was attributed to its good crystalline structure. The reaction products obtained from each of the three reaction runs were analyzed by <sup>13</sup>C NMR (Figure S9 of the Supporting Information). Peaks characteristic of furfural alone were observed in the hydrolysate after two regenerations of the catalyst. Moreover, the xylose conversion was complete. Thus, a reusable, active, and selective catalyst for the hydrolysis of xylose to furfural has been designed. Because the current process of furfural production from xylose uses  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> at modest loadings (0.4:1  $\beta$ -Ga<sub>2</sub>O<sub>3</sub>/ xylose ratio), a simple and surfactant-free catalyst is relatively

cheap. In addition, the use of  $\beta$ -Ga<sub>2</sub>O<sub>3</sub> facilitates the selective production of furfural from xylose. Because of the special features of this catalytic process, it can be used for industrial purposes.

# 4. CONCLUSION

A novel surfactant-free, acid-base free sonochemical pathway for the preparation of Ga<sub>2</sub>O<sub>3</sub> nanorods from molten Ga metal is reported. Combined sonication and calcination shortens the duration of the catalyst preparation (6 h) compared to conventional wet impregnation techniques. The  $\beta$ -Ga<sub>2</sub>O<sub>2</sub> catalyst exhibits good activity and selectivity in the conversion of xylose to furfural, which resulted in 94% yield of furfural with 66 wt % selectivity in 12 h at 150 °C. This catalyst was observed to be thermosensitive, which might be a key factor leading to higher production of furfural from xylose. This solid catalyst can be easily separated from the product and reused for the conversion of biomass to important platform chemicals. The detailed mechanism of the conversion of D-xylose to furfural is proposed. The chemical and thermosensitive behavior of the catalyst under the reaction conditions make it a reusable and potential catalytic system for industrial application in producing furfural from xylose. It is desirable to probe further into the kinetics of the process by measuring the rate of the reaction. These studies are now in progress.

# ASSOCIATED CONTENT

#### **Supporting Information**

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acs.energy-fuels.6b01568.

HRSEM, EDS, TEM, NMR, UV-vis, and XRD investigations of the catalyst and products (PDF)

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# Notes

The authors declare no competing financial interest.

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